

Hydrodynamics of laminar bubble chains

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& “Priroda” journal

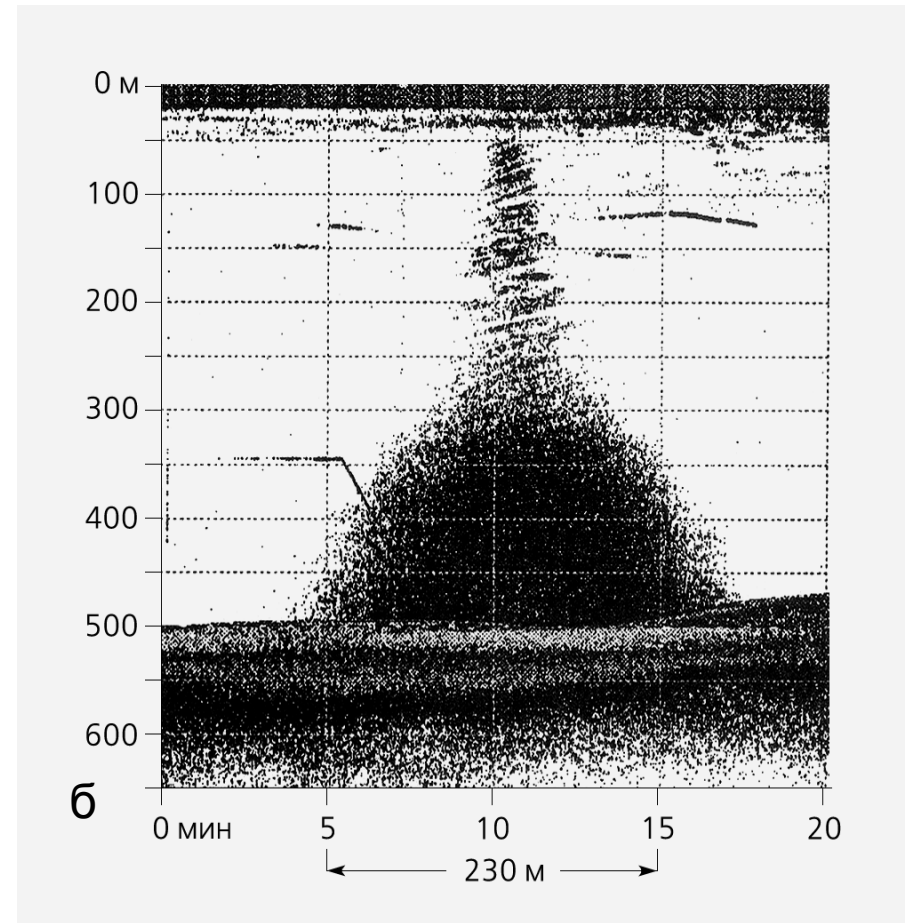
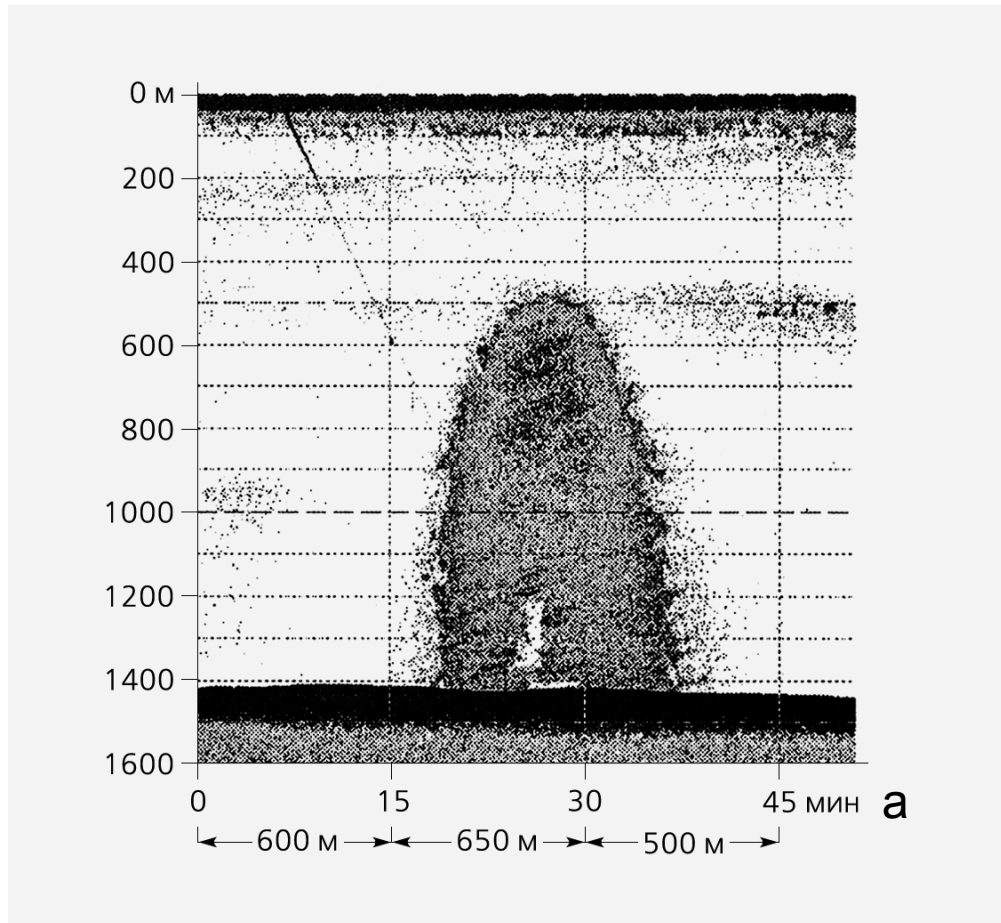
Abstract

A solution of hydrodynamic equations is obtained for the case of laminar bubble chains. Bubble sizes along the chain can either change both ways due to gas-liquid interactions or grow due to pressure decrease. The liquid velocity in region near chain axe occurs to be of the order of single bubble rise velocity.

Our final aim - explanation of methane flows

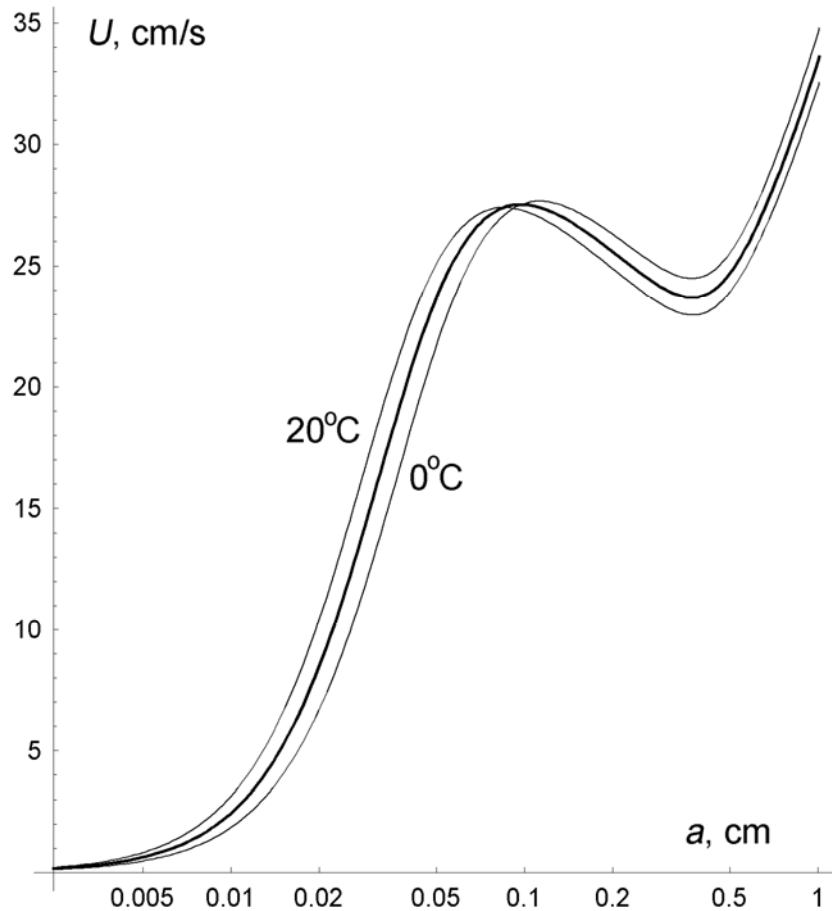
Exempls: ("Priroda", 2010, №3

Granin N.G, Makarov M.M., Kucher K.M., Gnatovsky R.Yu.)



a) Methane flow "Sankt-Peterbug", lake Baikal, October 2005.

b) Methane flow «Stupa», Baikal, cap Kadilny, August 2007.

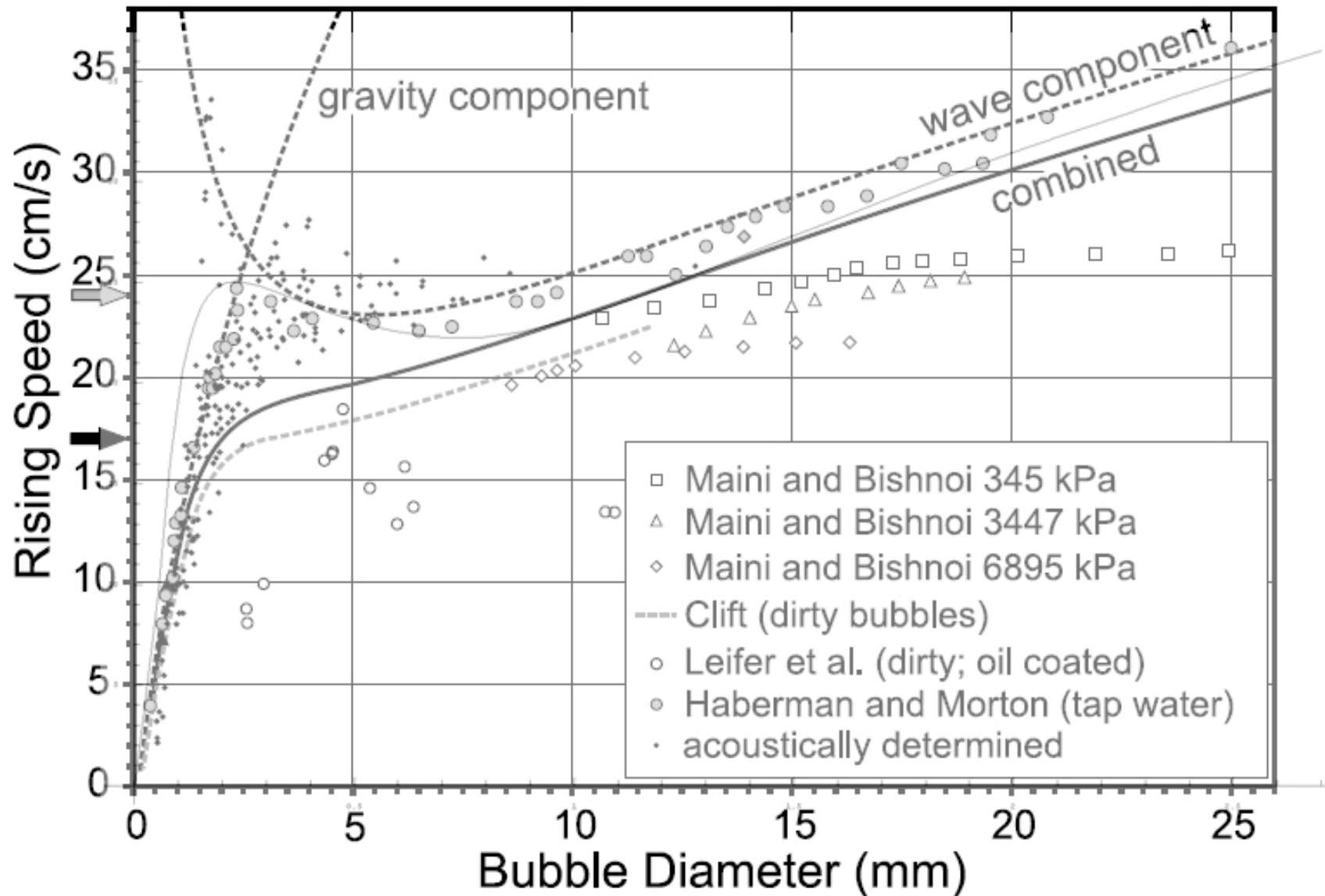


$$L_v = \nu^{2/3} g^{-1/3} = 0.0056 \text{ cm}$$

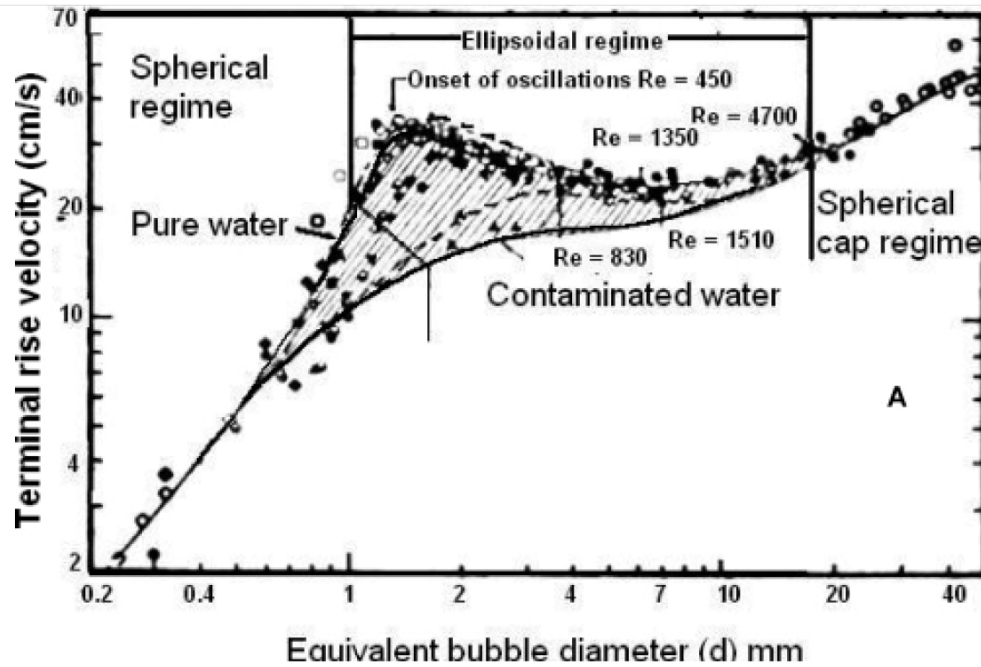
$$L_\sigma = \sqrt{\sigma/\rho g} = 0.207 \text{ cm}$$

Rodrigue D. A General Correlation for the Rise Velocity of Single Gas Bubbles// The Canadian Journal of Chemical Engineering, 2004, V. 82, 382—386:

$$U = \frac{ga^2}{3\nu} \frac{\left[1 + 7.817 \cdot 10^{-4} \left(\frac{L_v}{L_\sigma}\right)^{\frac{33}{10} + \frac{146}{99}} \left(\frac{a}{L_v}\right)^{8 + \frac{73}{99}} \right]^{\frac{21}{176}}}{\left[1 + 0.1073 \left(\frac{L_v}{L_\sigma}\right)^{\frac{20}{33}} \left(\frac{a}{L_v}\right)^{\frac{80}{33}} \right]^{\frac{10}{11}}}$$

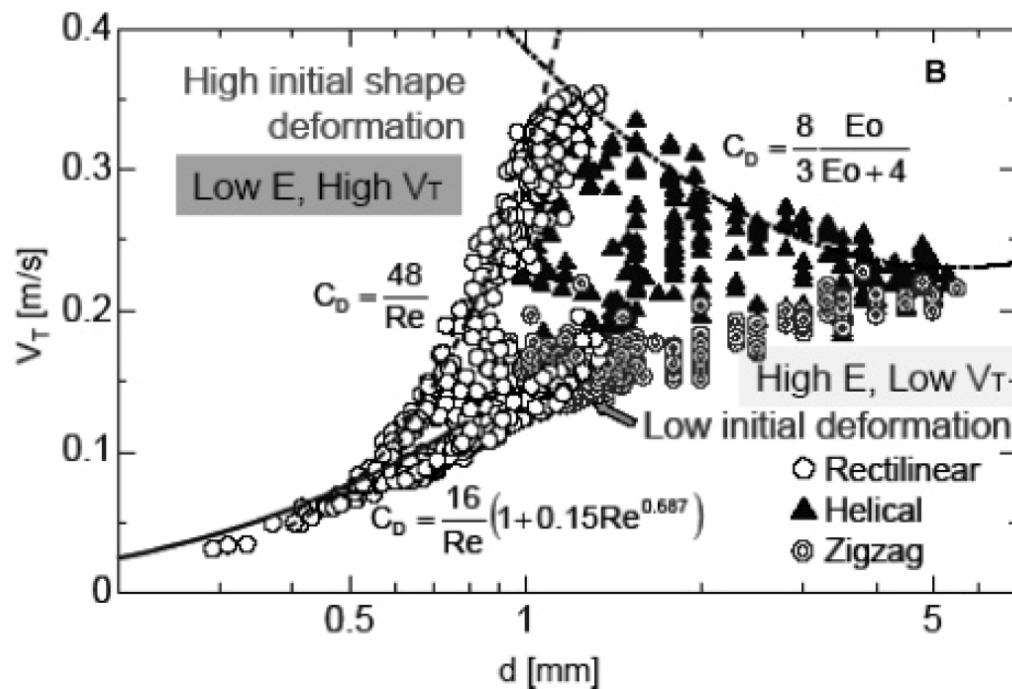


McGinnis D. F. et al. Fate of rising methane bubbles in stratified waters: How much methane reaches the atmosphere? *Journal of geophysical research*, Vol. 111, C09007.



Amol A. Kulkarni and Jyeshtharaj B. Joshi. Bubble Formation and Bubble Rise Velocity in Gas-Liquid Systems: A Review. *Ind. Eng. Chem. Res.* 2005, 44, 5873-5931

(A) Typical trends in rise velocity with bubble size for pure and contaminated liquids (reproduced with permission from Clift, R.; Grace, J. R.; Weber, M. E. *Bubbles, Drops, and Particles*; Academic Press: London, 1978).



(B) Effect of initial bubble deformation on terminal rise velocity in distilled water. (reproduced with permission from Tomiyama, A. *Drag, lift and virtual mass forces acting on a Single Bubble*, 3rd International Symposium on Two-Phase Flow Modelling and Experimentation, Pisa, 22-24 September 2004. E - distortion factor, C_D - drag coefficient

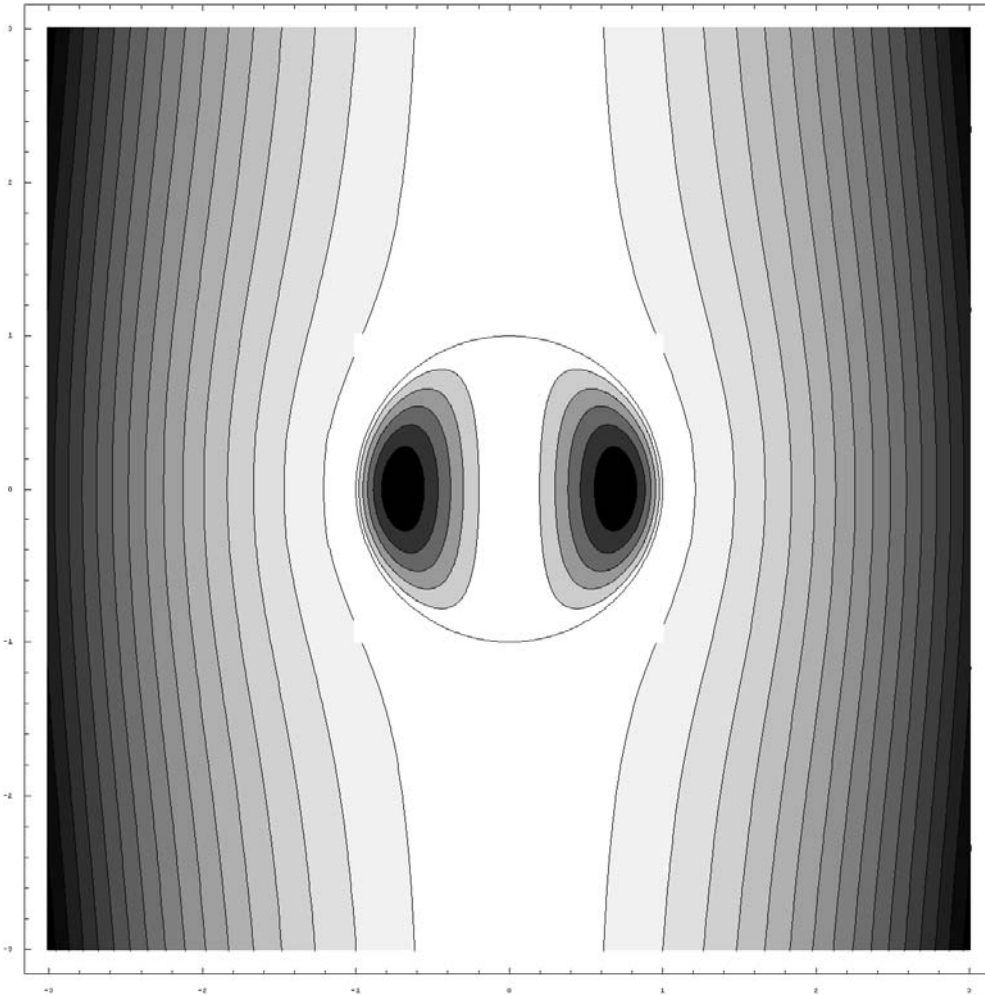
Potential ψ

[Van Dyke M. Perturbation methods in fluid dynamics.
Academical Press, 1964.]

$$v_r = \frac{1}{r^2 \sin(\vartheta)} \frac{\partial \psi}{\partial \vartheta}; \quad v_\vartheta = -\frac{1}{r \sin(\vartheta)} \frac{\partial \psi}{\partial r}.$$

The continuity equation fulfills automatically in such approach.
Dimension of potential coincides with dimension of flow i.e. cm³/s.
Surfaces of constant potential correspond to lines of flow.
In the bubble system of reference the total flow thru removed surface is zero:

$$\lim_{r \rightarrow \infty} 2\pi r^2 \int_0^\pi v_r \sin \vartheta \, d\vartheta = \lim_{r \rightarrow \infty} [\psi(r, \pi) - \psi(r, 0)] 2\pi = 0.$$



The Stokes—Rybchinsky solution. Lines of flow in around a bubble in the bubble reference system.

The term $\frac{U}{2}r^2\sin^2(\vartheta)$

corresponds to the uniform flow with velocity

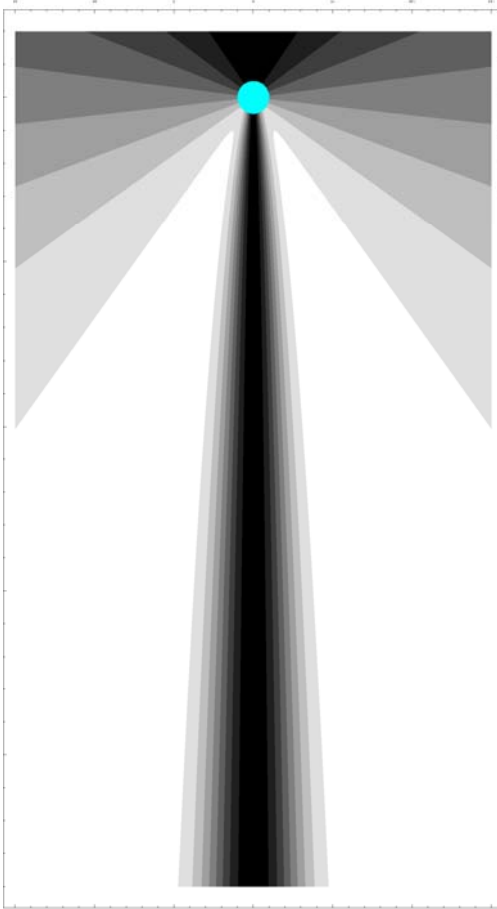
$$U(a) = \frac{ga^2}{3\nu}$$

The drag force equals to Archimedes force:

$$\psi_{\text{in}}(r, \vartheta) = \frac{U}{4a^2}r^2(r^2 - a^2)\sin^2(\vartheta);$$

$$\psi_{\text{out}}(r, \vartheta) = \frac{U}{2}r(r - a)\sin^2(\vartheta).$$

$$F = 4\pi\rho\nu Ua = \frac{4\pi}{3}g\rho a^3; \quad U(a) = \frac{ga^2}{3\nu}.$$



Oseen solution

$$\psi_a(r, \vartheta) = -av(1 + \cos\vartheta) \left\{ 1 - \exp \left[-\frac{Ur}{2\nu} (1 - \cos\vartheta) \right] \right\}$$

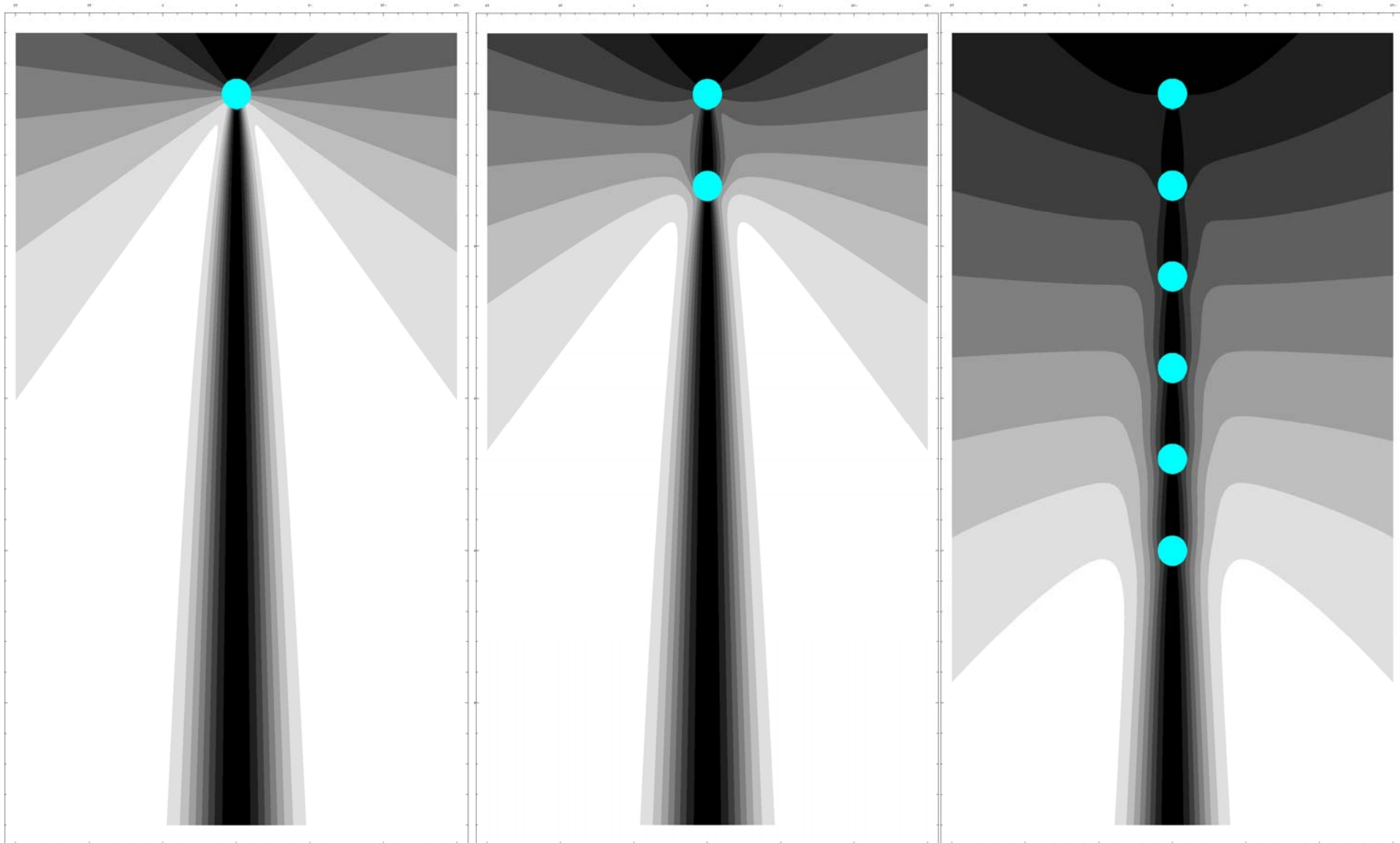
At small distances $r \ll \nu/U$ the Oseen and Rybchinsky expressions coincide, but the Oseen solution does not satisfy boundary conditions at $r = a$.

Simultaneously the Oseen region of applicability is much wider, it can be applied in the region $r \gg aR$ for any Reynolds numbers $R = Ua/\nu$.

An equivalent form of Oseen solution:

$$\psi_a(r, \vartheta) = -\frac{F(a)}{2\pi\rho U(a)} \cos^2 \frac{\vartheta}{2} \left[1 - \exp \left(-\frac{U(a)r}{\nu} \sin^2 \frac{\vartheta}{2} \right) \right].$$

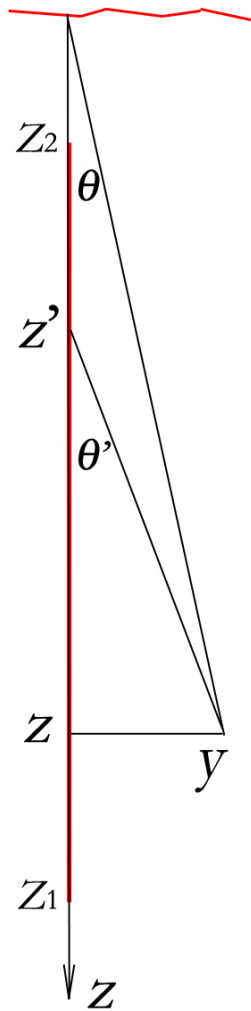
$$F(a) = \frac{4\pi}{3} g\rho a^3.$$



$$\psi(r, \vartheta) = \sum_a \psi_a(r, \vartheta) \approx \frac{1}{\tau} \int_{z_1}^{z_2} \frac{dz'}{U' + V'} \psi_a(r', \vartheta').$$

$$D = \tau(U + V) \gg a$$

Short uniform bubble chain



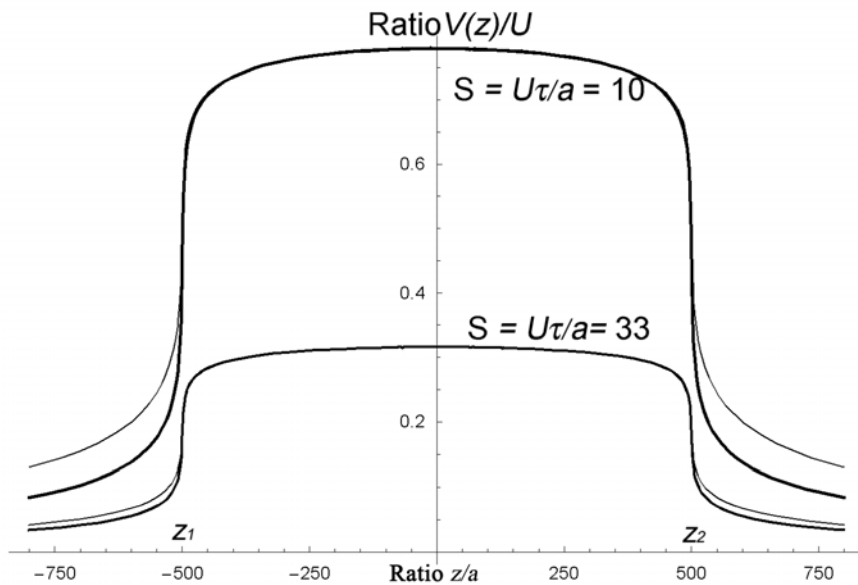
$$\psi(r, \vartheta) = -\frac{2g}{3\tau} \int_{z_2}^{z_1} \frac{a^3 dz'}{U[U + V(z')]} \cos^2 \frac{\vartheta'}{2} \left[1 - \exp\left(-\frac{Ur'}{v} \sin^2 \frac{\vartheta'}{2}\right) \right].$$

$$y = r \sin \vartheta = r' \sin \vartheta' = (z - z') \operatorname{tg} \vartheta';$$

$$dz' = \frac{y}{\sin^2 \vartheta'} d\vartheta'; \quad r' = \sqrt{y^2 + (z - z')^2}.$$

$$V(z) = -\lim_{y \rightarrow 0} \frac{\partial \psi(y, z)}{y \partial y} = \frac{g}{3\tau v} \lim_{y \rightarrow 0} \int_{z_1}^{z_2} dz' \frac{a^3}{[U + V] \sqrt{y^2 + (z - z')^2}}.$$

$$V^2 + UV - \frac{ga^3}{3\tau\nu} L(z) = 0; \quad L(z) = \ln \left(\frac{-z + z_1 + \sqrt{(-z + z_1)^2 + a^2}}{-z + z_2 + \sqrt{(-z + z_2)^2 + a^2}} \right).$$



$$V(z, \tau) = -\frac{U}{2} + \sqrt{\frac{ga^3}{3\tau\nu} L(z) + \frac{U^2}{4}}$$

$$U = \frac{a^2 g}{3\nu} \ll \frac{aL}{\tau} \text{ then } V \cong \sqrt{\frac{aU}{\tau} L(z)} < U.$$

Functions $V(z)/U$ in two approximations
for $S = U\tau/a = 10$ and $S = U\tau/a = 33$
 $z_1 = -500$; $z_2 = 500$ (in bubble sizes)

$$\frac{a^2}{\tau\nu} \ll 1, \quad \text{then } V \cong U \sqrt{\frac{a^2}{3\tau\nu} L(z)} < U.$$

Laminar flow condition:

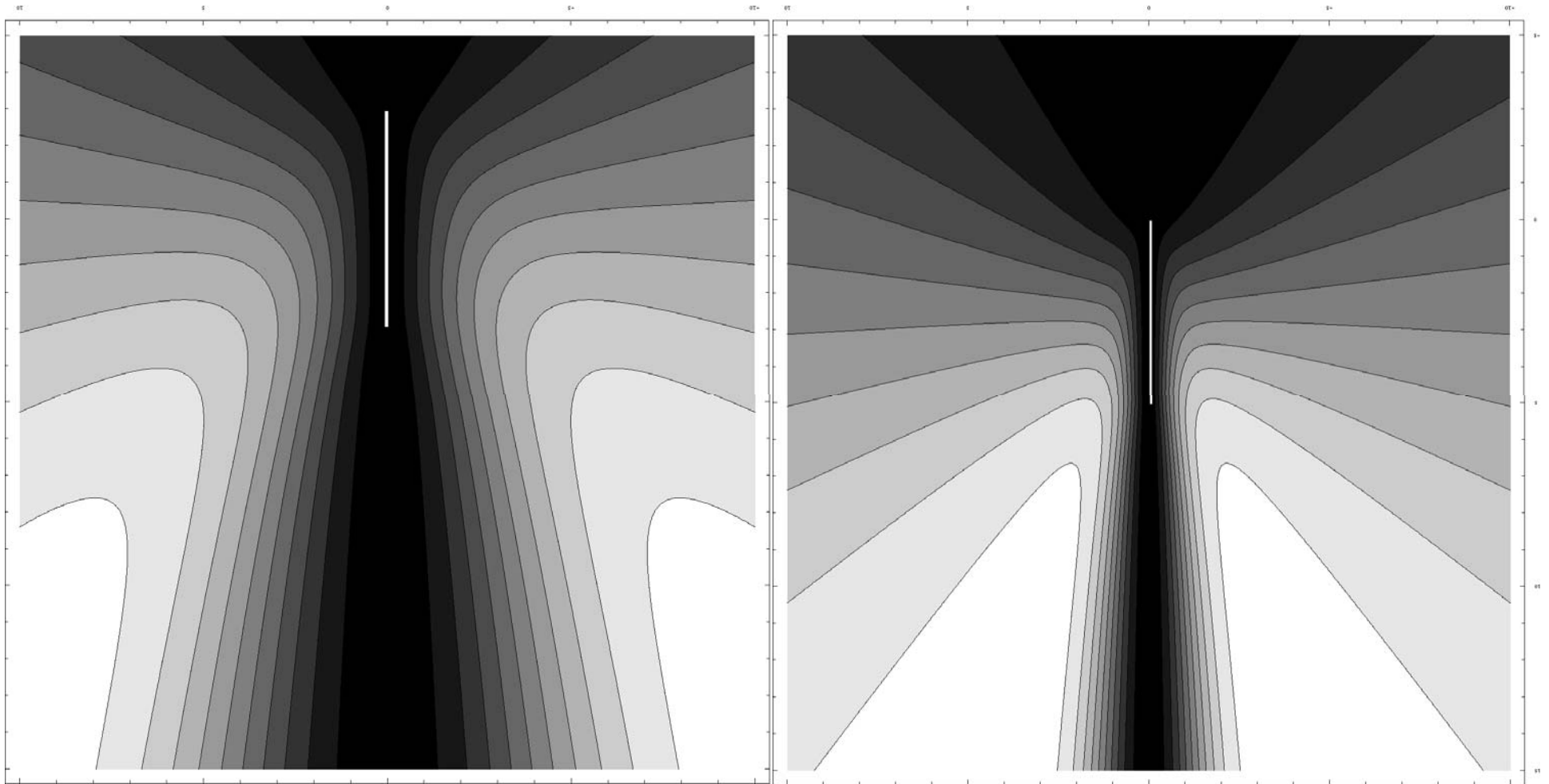
Short uniform bubble chain

$$\psi(r, \vartheta) = -\frac{2g}{3\tau} \int_{z_2}^{z_1} \frac{a^3 dz'}{U[U + V(z')]} \cos^2 \frac{\vartheta'}{2} \left[1 - \exp\left(-\frac{Ur'}{v} \sin^2 \frac{\vartheta'}{2}\right) \right].$$

$$\xi = \frac{Uy}{2v} \operatorname{tg} \frac{\vartheta'}{2} = \frac{U}{2v} \left(\sqrt{(z - z')^2 + y^2} - z + z' \right).$$

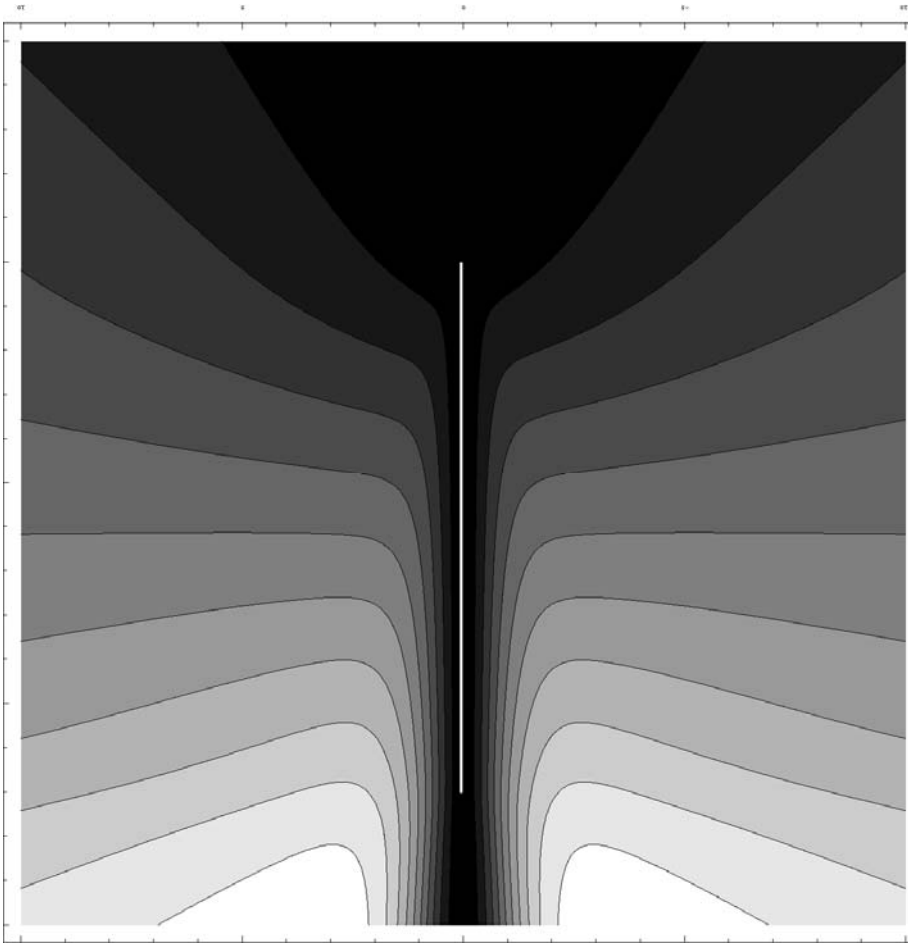
$$\psi(z, y) = \frac{ga^3 y^2}{6v\tau[U(a) + V(z)]} \left[\frac{1 - \exp(\xi_1)}{\xi_1} \operatorname{Ei}(-\xi_1) - \frac{1 - \exp(\xi_2)}{\xi_2} \operatorname{Ei}(-\xi_2) \right],$$

$$\text{where } \xi_{1,2} = \frac{u}{2v} \left(\sqrt{(z - z_{1,2})^2 + y^2} - z + z_{1,2} \right).$$

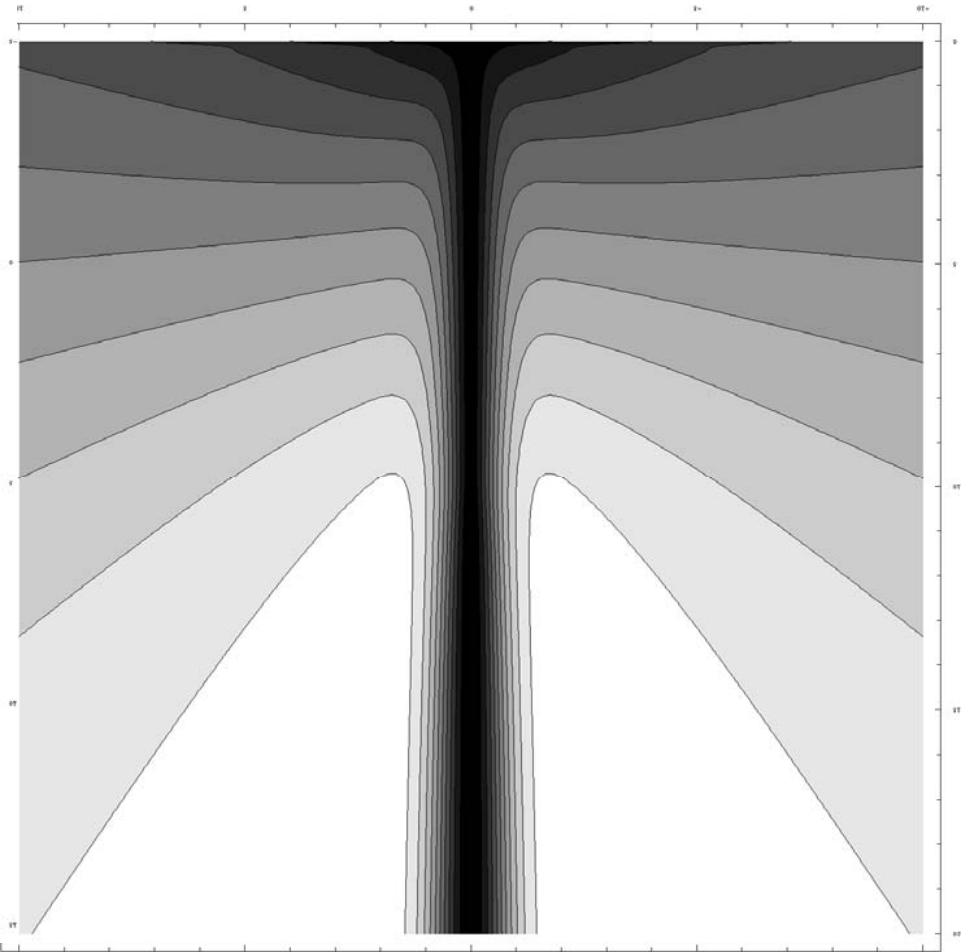


Flow around a short chain (white in center, $R=1$)

•Flow around a short chain (white in center, $R=10$, $\Delta z=5$)

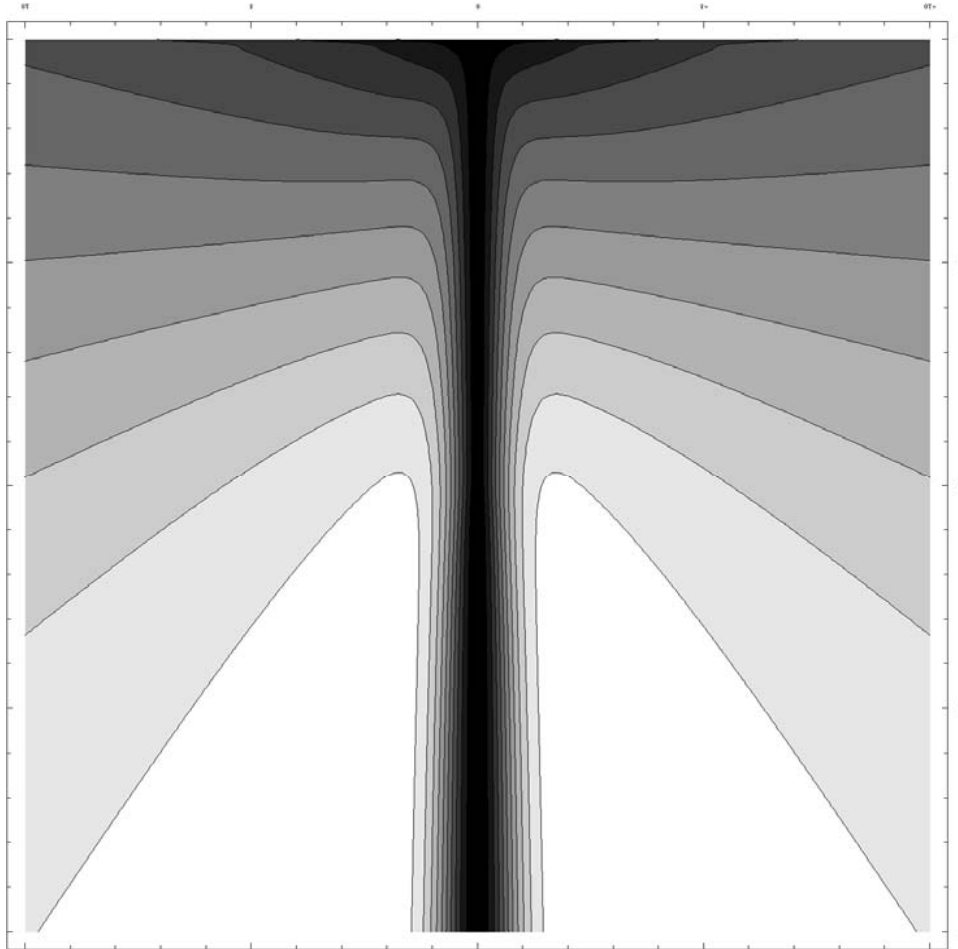


Lines of flow around a chain
 (white in center, $R=10$,
 $\Delta z=12$)



Lines of flow for “dying” chain
 real sizes (10x10 cm);
 $a_0 = 0.005$ cm. $z_1 = 10$ cm.

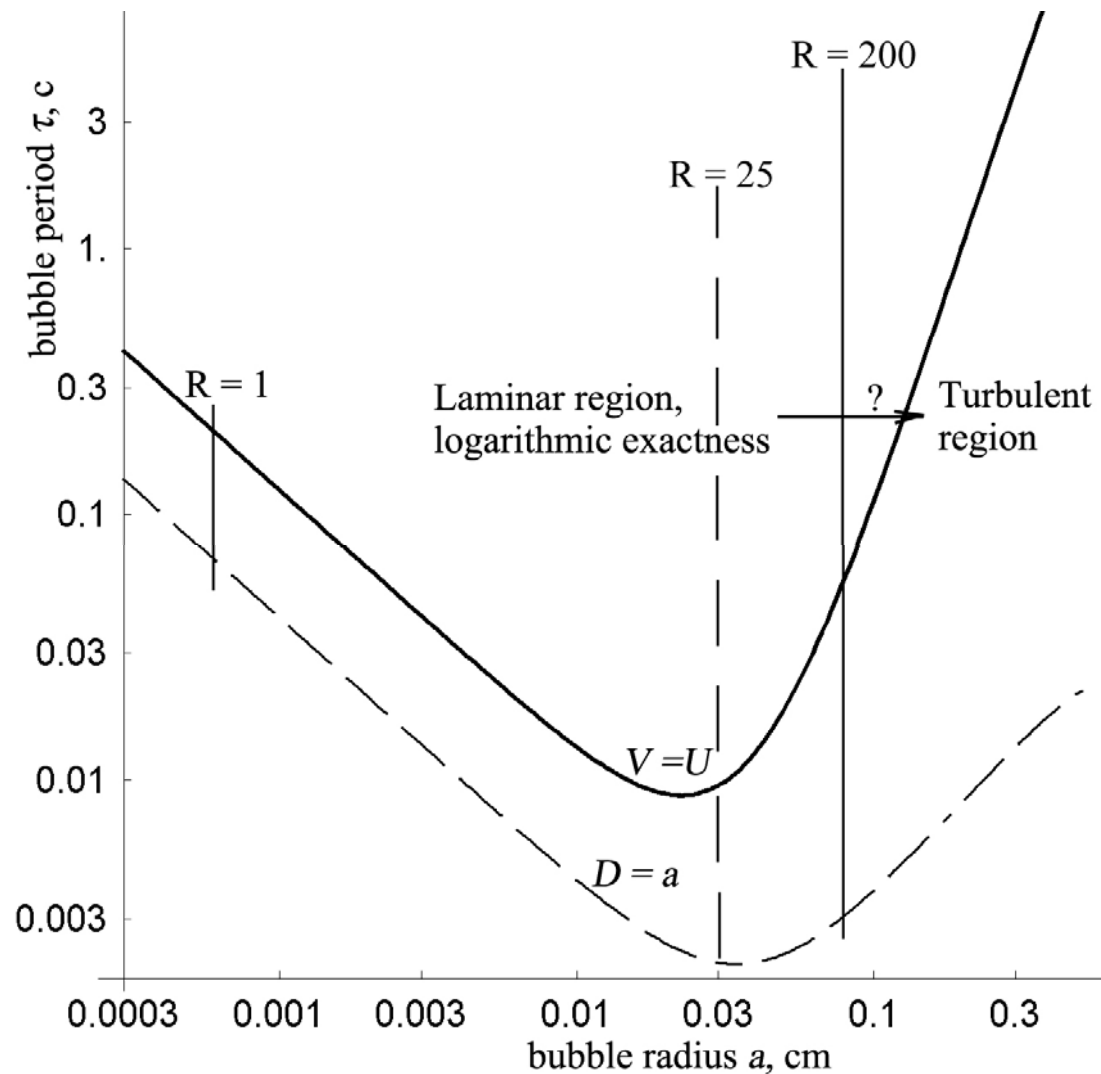
Dying chain



$$a = \left(\frac{\nu K z}{g} \right)^{1/3} ; U(z) = \frac{1}{3} \left(\frac{K^2 g z^2}{\nu} \right)^{1/3}$$

The absorption coefficient
 $K = (1.0—1.05)10^{-3}$ cm/s.

$$\psi(z, y) = \frac{3\nu^{5/3}}{K^{1/3} g^{2/3} \tau} \int_0^{z_1} \frac{dz'}{z'^{2/3}} \left(1 + \frac{(z - z')}{\sqrt{y^2 + (z - z')^2}} \right) \left\{ 1 - \exp \left[-\frac{1}{6} \left(\frac{K^2 g z^2}{\nu^4} \right)^{1/3} \left[\sqrt{y^2 + (z - z')^2} - (z - z') \right] \right] \right\}$$



Limits of chain solution applicability:

$D = U\tau \gg a$: Chain region; $V \leq U$: Region of logarithmic exactness.

$R = aU/\nu < 25$: Laminar region; $U(a)$ well defined;

$25 < R < 200$: Laminar region; U depends on bubble distortion

Applicability to turbulent bubble rise ($R > 200$) is questionable.

Bubble “pump”

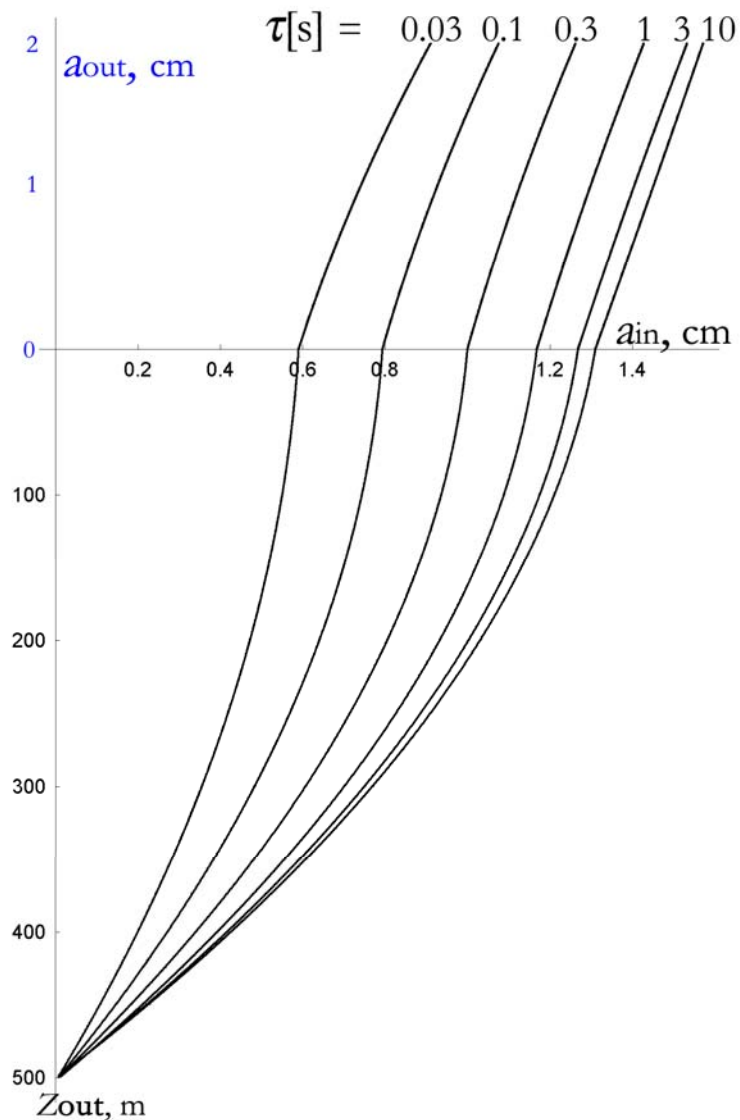
$$\lim_{r \rightarrow \infty} 2\pi r^2 \int_0^{\pi/2} v_r \sin \vartheta \, d\vartheta = \lim_{r \rightarrow \infty} \left[\psi_a(r, \pi) - \psi_a\left(r, \frac{\pi}{2}\right) \right] 2\pi = -\frac{2\pi g a^3}{3U(a)},$$

$$\Phi_{\text{liq}} = \frac{2\pi g}{3\tau} \int_0^{z_1} dz \frac{a^3}{U(U+V)}, \quad \Phi_{\text{gas}} = \frac{4\pi g a_1^3}{3\tau} \quad \text{where} \quad a_1 = a(z_1)$$

$$a^3(z + z_0) = \text{const}$$

$$\frac{\Phi_{\text{liq}}}{\Phi_{\text{gas}}} = \frac{gz_0}{2} \int_0^{z_1} \frac{dz}{(z + z_0)U(U+V)} \sim \frac{gz_0}{\langle U^2 \rangle} \sim 10^2.$$

An attempt to use laminar results in the turbulent region.



The absorption coefficient

$$K = (1.0—1.05)10^{-3} \text{ cm/s.}$$

p_0 is atmospheric pressure,

$$p_0/\rho g = 10 \text{ m.}$$

$$\frac{da}{dz} = \frac{K}{U(a) + V(z, \tau)} - \frac{a}{3(z + p_0/\rho g)}$$

Long methane bubble chains starting at depth 500 m.

Final depth (lower scale) or size after reaching the sea surface (upper scale) in dependence on bubble period τ and their initial size a_{in} .